



A Particle-based Model of Flow-Induced Scour

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Outline



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Introduction



- Experimental observations show that if the fluid flow velocity exceeds a certain value, the particles in the upper layers of the bed would start moving (sheet flow).
- There is a lack of understanding of many characteristics of the particles and fluid interaction especially the top layers of particles (sheet flow layer).

No-slip Boundary

Sheet Flow Layer Stationary Particles Bed



Introduction



- The interaction between the fluid and solid phases involves high fluid velocities and transient variations in the properties of the fluid and solid phases as the erosion occurs.
- We present a three-dimensional fully coupled transient fluid-particle model to simulate flood-induced erosion of a particle bed.
- A parallel experimental program provides pore-scale fluid velocity using digital particle image velocimetry (DPIV) for comparison with the numerical results.
- We present the response of a particle bed to Poiseuille flow conditions to get a better understanding of the dynamics of the sheet flow layer by tracking particle and fluid velocities.





Coupled Fluid Particle Model

Continuum fluid phase:

- Solved using FEM code
- Averaged Navier-Stokes equations (Jackson, 2000; El Shamy 2004):

Continuity

$$\frac{\partial \boldsymbol{n}}{\partial t} + \nabla . \left(\boldsymbol{n} \overline{\boldsymbol{v}}_f \right) = 0$$

Momentum

 $\rho_f \left(\frac{\partial (n\bar{\mathbf{v}}_f)}{\partial t} + \nabla . (n\bar{\mathbf{v}}_f \bar{\mathbf{v}}_f) \right) = -n\nabla \bar{p}_f \delta + \mu_f \nabla^2 (n\bar{\mathbf{v}}_f) - \bar{\mathbf{f}}_{f-p} + n\rho_f \mathbf{f}_g$ $\bar{\mathbf{f}}_{f-p}: \text{Fluid-particle interactions}$



Fluid Phase

Forces applied by the fluid on the particles: Drag force f_{drag} (*Di Felice*, 1994; Xu, 1997):

$$\mathbf{f}_{drag} = \left(\frac{1}{8} C_d \rho_f \pi d_p^2 |\mathbf{v}_f - \mathbf{v}_p| (\mathbf{v}_f - \mathbf{v}_p)\right) n^{-\chi}$$

• Lift force \mathbf{f}_l (Saffman, 1965 & 1968):

$$\mathbf{f}_l = 1.62 (\mathbf{v}_f - \mathbf{v}_p) d_p^2 \sqrt{\rho_f \mu_f u^*} \operatorname{sgn}(\mathbf{u}^*)$$

$$\bar{\mathbf{f}}_{f-p}^{i} = \frac{\sum_{j} (\mathbf{f}_{drag}^{j} + \mathbf{f}_{l}^{j})}{V_{i}}$$
$$\mathbf{f}_{fluid} = (\mathbf{f}_{drag} + \frac{1}{6} \pi d^{3} \nabla \bar{\mathbf{p}}_{f}) + \mathbf{f}_{l}$$







Coupled Fluid Particle Model



Discrete solid phase:

- Solved using DEM code
- Newton's second law of motion :

Linear momentum
$$m_p \ddot{\mathbf{u}}_p = m_p \mathbf{f}_g + \sum_{c=1}^{N_c} \mathbf{f}_c + \mathbf{f}_{fluid}$$

Angular momentum

$$I_p \ddot{\boldsymbol{\Theta}}_p = \sum_{c=1}^{N_c} \mathbf{r}_c \times \mathbf{f}_c$$



Experimental Setup



- Fluid velocity was obtained using *digital particle image velocimetry* (DPIV).
- The fluid used in the experiment was an aqueous solution of *sodium iodide* and *sodium thiosulfate*.
- The *sodium iodide* increases the refractive index of the solution to be nearly the same as the solid beads in order to measure the fluid velocity using DPIV technique.
- The sodium thiosulfate prevents discoloration of the solution.







Simulation Data



Particles (Pyrex)	
Number	11639
Diameter	3 mm
Density	2230 kg/m ³
Normal Stiffness	1×10 ⁵ N/m
Shear Stiffness	$1 \times 10^5 \mathrm{N/m}$
Friction Coefficient	0.5
Wall	
Normal Stiffness	1×10 ⁵ N/m
Shear Stiffness	1×10 ⁵ N/m
Friction Coefficient (side walls)	0.05
Friction Coefficient (base wall)	0.5
Fluid	
Density	1750 kg/m ³
Kinematic Viscosity	1.42×10 ⁻⁶ m ² /s

Particle Bed Erosion







Particles Snapshots



Experimental





Particle bed





Fluid Flow Velocity







Particles Velocity







Conclusions



- The dynamics of a particle bed subjected to flood-induced erosion was studied using a fully coupled numerical model.
- FEM was used to model the fluid and DEM was used to model the bed particles.
- An experimental program utilizing DPIV provided pore-scale fluid velocity.
- The numerical and experimental fluid and particle velocity profiles were in good agreement.
- The numerical and experimental results show that the fluid flow profile penetrates the bed for a small distance known as sheet flow layer.
- It is the relative velocity between the fluid penetrating the bed and the initially static particles that contributes to flow-induced drag and lift forces that cause particles to deform in response to these external forces.



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Questions?